

Supporting Information for

## **Novel Insights into Energy Storage Mechanism of Aqueous**

### **Rechargeable Zn/MnO<sub>2</sub> Batteries with Participation of Mn<sup>2+</sup>**

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## **Discussion S1 Density Functional Theory Calculation**

Density functional theory (DFT) calculations were performed with the Vienna ab-initio simulation package with projector augmented wave pseudo-potentials. The Perdew-Burke-Ernzerhof exchange-correlation functional is used with the Hubbard U-corrections to correct the self-interaction error introduced by the highly localized *d* orbitals. In our calculations, the parameter of U-J=3.9 eV was employed. The cut-off for the plane wave basis set was 520 eV and a minimum of 3\*3\*5 gamma-centered k-point mesh was used. The calculated crystal structures were visualized using the program Visualization for Electronic and Structural Analysis. The relaxation of one Zn<sup>2+</sup> into one  $\alpha$ -MnO<sub>2</sub> cell was carried out. Before the DFT calculation,  $\alpha$ -MnO<sub>2</sub> cell has been relaxed. Calculation results are in Table S5.

## **Discussion S2 Theoretical Analysis of MnO<sub>2</sub> as a Cathode in the Aqueous Zinc-ion Battery**

The anode potential ( $\psi^-$ ) is equal to the equilibrium potential of zinc dissolution and deposition.  $\psi^- = -0.763$  V vs standard hydrogen electrode for the depth of discharge.

$a_{Zn^{2+}} = 0.14$  (ion activity of  $Zn^{2+}$  is calculated, as shown in Eqs. S3-S5). The pH value of electrolyte is 5.5 (Fig. S13) [S1] at which  $ZnSO_4 \cdot 3Zn(OH)_2 \cdot 5H_2O$  (noted as “BZSP”) would be produced. There are six theoretical electrochemical reduction progresses of  $MnO_2$  in Mn-Zn- $H_2O$  system (Table S6). The cathode potential is calculated by the Nernst equation. The cathode potential descends continuously when the homogeneous reaction occurs. The cathode potential keeps constant when the heterogeneous reaction happens, while changes of ion activity and pH value are ignored. If the anode potential also keeps constant, there would be a platform in the constant voltage charge/discharge curve. These six reduction reactions differ from the theoretical reductive phases, the potential of the reaction or the shape of batteries’ constant voltage charge/discharge curve. The reductive phase of active materials, the potential of the reaction and the shape of batteries’ constant voltage charge/discharge curve are determined by experiment. As such, the discharge mechanism of  $MnO_2$  as the cathode can be figured out.

$$\Delta E_f = E_{\alpha-Zn_xMnO_2} - xE_{Zn} - E_{\alpha-MnO_2} \quad (S1)$$

$$E_f = \Delta G_f / zF \quad (S2)$$

In which  $\Delta G_f$  is Gibbs free energy change of the reaction,  $z$  is electron transfer number and  $F$  is Faraday constant.  $\Delta G_f$  can be calculated by the data in Table S7.  $\Delta E_f$  is the formation of energy calculated by DFT.

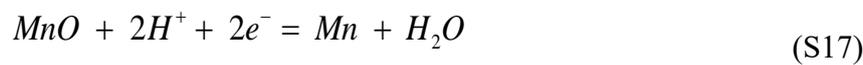
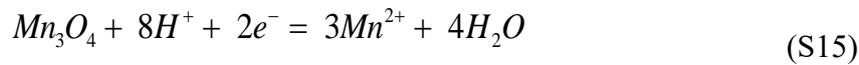
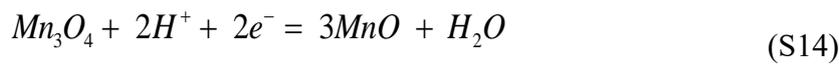
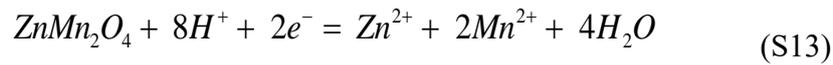
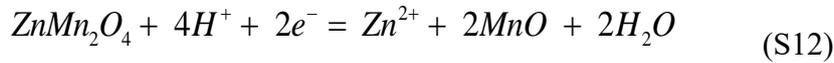
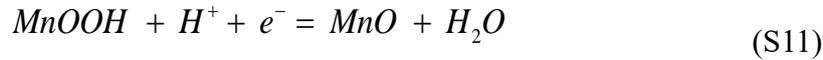
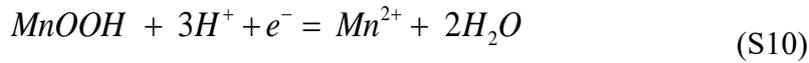
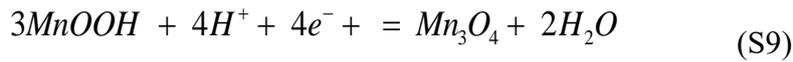
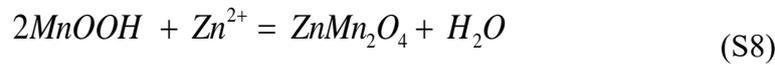
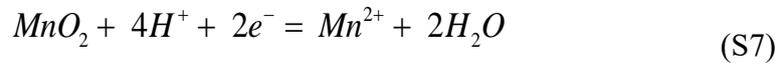
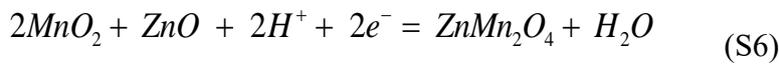
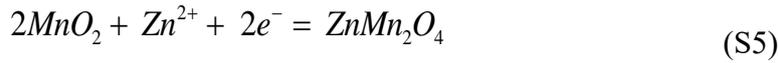
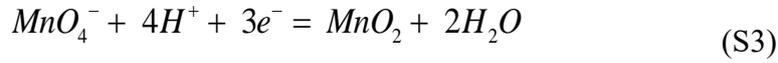
From the experimental evidence, the take-off potential of  $R_2$  is about 1.5 V vs.  $Zn^{2+}/Zn$  and the battery voltage descends continuously, the take-off potential of  $R_1$  is about 1.35 V and the battery voltage keeps nearly constant,  $\alpha-Zn_xMnO_2$  or  $ZnMn_2O_4$  would be produced during  $R_2$  and  $MnOOH$  or  $Mn_2O_3$  would be generated during  $R_1$ .

Batteries’ voltage would be lower than the theoretical electromotive force due to the polarization. Thus, combined with the shape of constant voltage charge/discharge curve and the reductive phase, it can be concluded that heterogeneous reaction would occur during  $R_1$  of initial discharge progress and the discharge mechanism in  $R_1$  is proton-electron conversion mechanism or manganese oxide conversion mechanism. It can be also concluded that homogeneous reaction occurs in  $R_2$  and the discharge mechanism in  $R_2$  is zinc ion insertion mechanism and the final reductive phase is  $ZnMn_2O_4$ . That is, the peak at 1.3-1.5 V vs  $Zn^{2+}/Zn$  in cyclic voltammetry (CV) curve indicates the zinc ion insertion reaction, while the peak at 1-1.3 V indicates the reaction in which proton participated.

The formation of BZSP,  $MnOOH$ ,  $Mn_2O_3$ ,  $Mn^{2+}$  (aq),  $\alpha-Zn_xMnO_2$  or  $Zn_2Mn_4O_8 \cdot H_2O$  is detected by experiment. Among these, the formation of  $Mn^{2+}$  (aq) is due to the reduction or the disproportionation of trivalent manganese ion (manganese in

MnOOH or Mn<sub>2</sub>O<sub>3</sub>). The formation of Mn<sub>2</sub>O<sub>3</sub> is not the result of manganese oxide conversion mechanism but the production of dehydration of MnOOH. Zinc ion insertion reaction results in  $\alpha$ -Zn<sub>x</sub>MnO<sub>2</sub> and  $\alpha$ -Zn<sub>x</sub>MnO<sub>2</sub> may transfer to ZnMn<sub>2</sub>O<sub>4</sub>. Thus, the following reactions may occur during the process as shown in 2.1:

### S2.1 Reactions for Calculation of Pourbaix Diagrams



### S2.2 Calculation of Zinc-ion Activity

Ionic activity coefficient is calculated by Eq. S19:

$$\lg \gamma_i = \frac{-Az_i^2 \sqrt{I}}{1 + BR_i^H \sqrt{I}} \quad (\text{S19})$$

in which  $\gamma_i$  is activity coefficient,  $I$  is ionic strength,  $z_i$  is in charge of the ion,  $R_i^H$  (angstrom) is hydrated ion size of the ion, A and B are coefficient (At 25 °C in aqueous solutions, A and B are 0.5115 and 0.3291, respectively).

$I$  is calculated by Eq. S20:

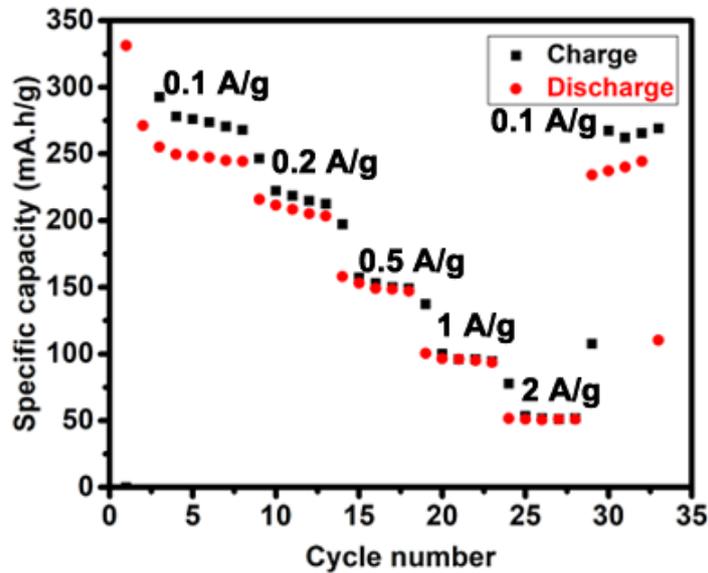
$$I = \frac{1}{2} \sum c_b z_b^2 \quad (\text{S20})$$

$c_b$  is the molar concentration of ion  $b$  in solution.  $z_b$  is the charge of ion  $b$  in solution.

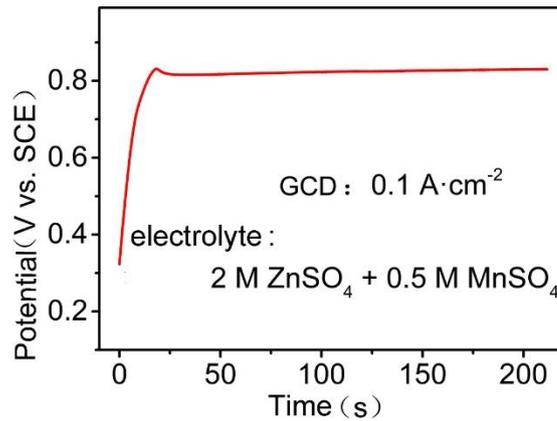
Zinc-ion activity is calculated by Eq. S21:

$$a_{\text{Zn}^{2+}} = \gamma_{\text{Zn}^{2+}} \cdot c_{\text{Zn}^{2+}} \quad (\text{S21})$$

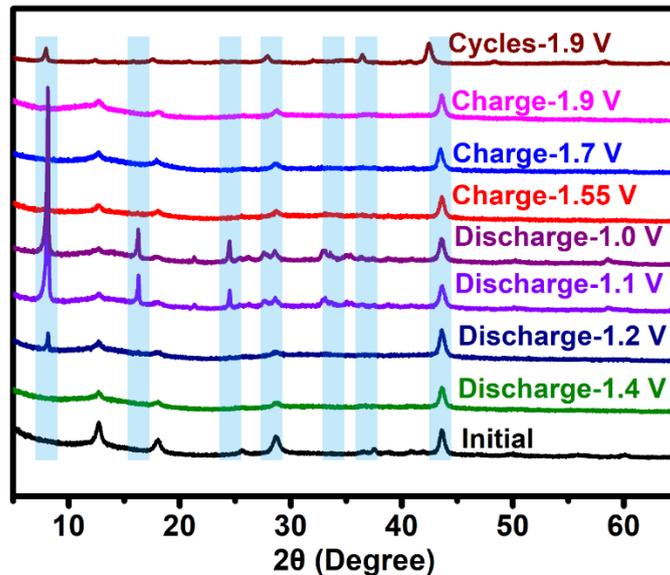
In 2 mol L<sup>-1</sup> ZnSO<sub>4</sub> solution,  $I = 8$ ,  $R_{\text{Zn}^{2+}}^H = 4.3$  angstrom<sup>2</sup>,  $R_{\text{Mn}^{2+}}^H = 4.38$  angstrom  
 $c_{\text{Zn}^{2+}} = 2$ ,  $z_{\text{Zn}^{2+}} = 2$ . So,  $\gamma_{\text{Zn}^{2+}} = 0.07$   $a_{\text{Zn}^{2+}} = 0.14$



**Fig. S1** Rate capabilities and cycling performances of the battery in 2 M ZnSO<sub>4</sub> + 0.5 M MnSO<sub>4</sub> system

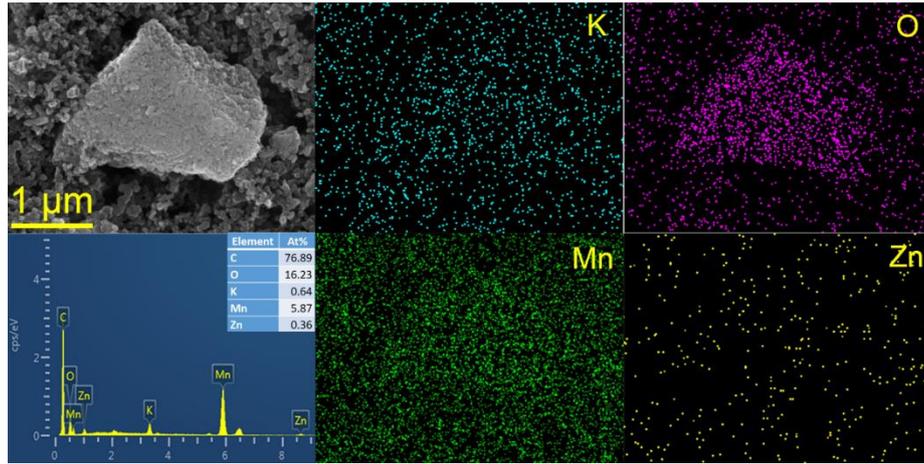


**Fig. S2** Potential vs. saturated calomel electrode (SCE) of the electro-deposition of  $\text{Mn}^{2+}$  in  $2 \text{ M ZnSO}_4 + 0.5 \text{ M MnSO}_4$  at a constant current of  $0.1 \text{ A cm}^{-2}$

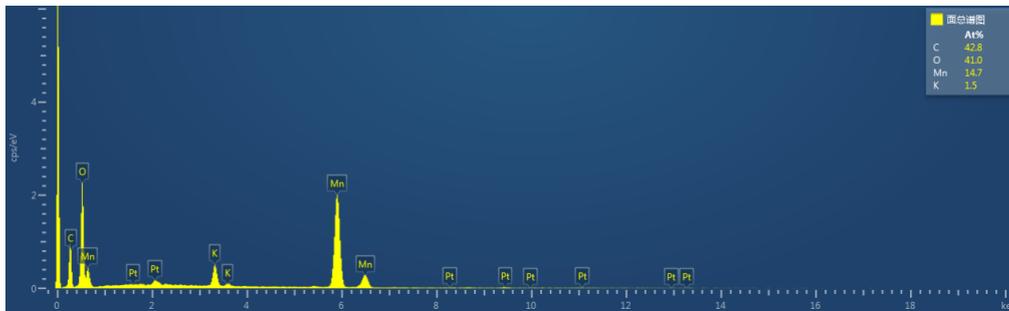


**Fig. S3** XRD of the cathodes at different charge/discharge states

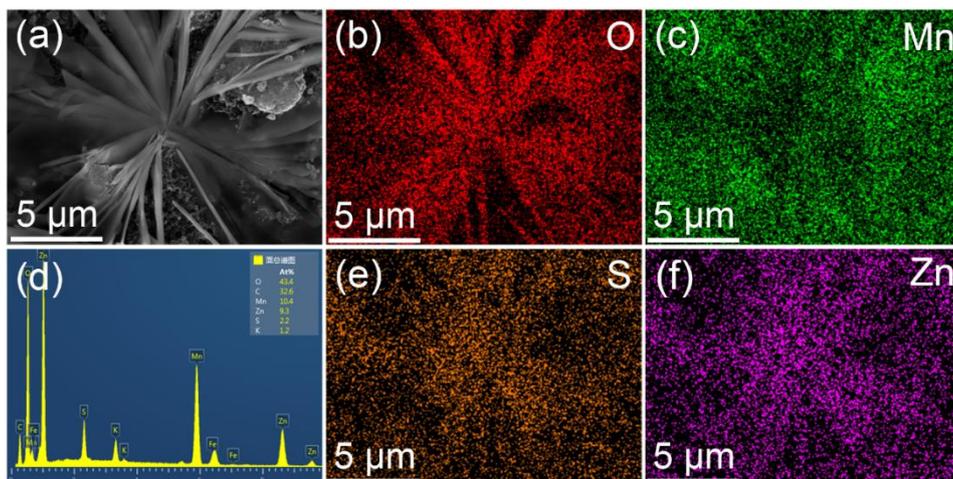
When the cathode is discharged to 1.4 V, no new phase produces. Nevertheless, characteristic peaks of the  $\text{MnO}_2$  active material such as the peaks at  $28^\circ$  and  $44^\circ$  shift, which is attributed to the change of the layer spacing of  $\text{MnO}_2$ . When the battery is further discharged to 1.2 and 1.0 V at constant current, several new diffraction peaks appear and then become stronger, especially the peaks at  $8^\circ$  and  $16^\circ$ , implying the generation of new phases. In charging process, some diffraction peaks cannot be detected, which means the disappearance of some phases. After 100 charge/discharge cycles, the XRD pattern is not in conformity with the XRD patterns of the cathode at original state and fully charged state in the 1st charge process (e.g., the diffraction peaks at around  $36^\circ$  and  $44^\circ$ ).



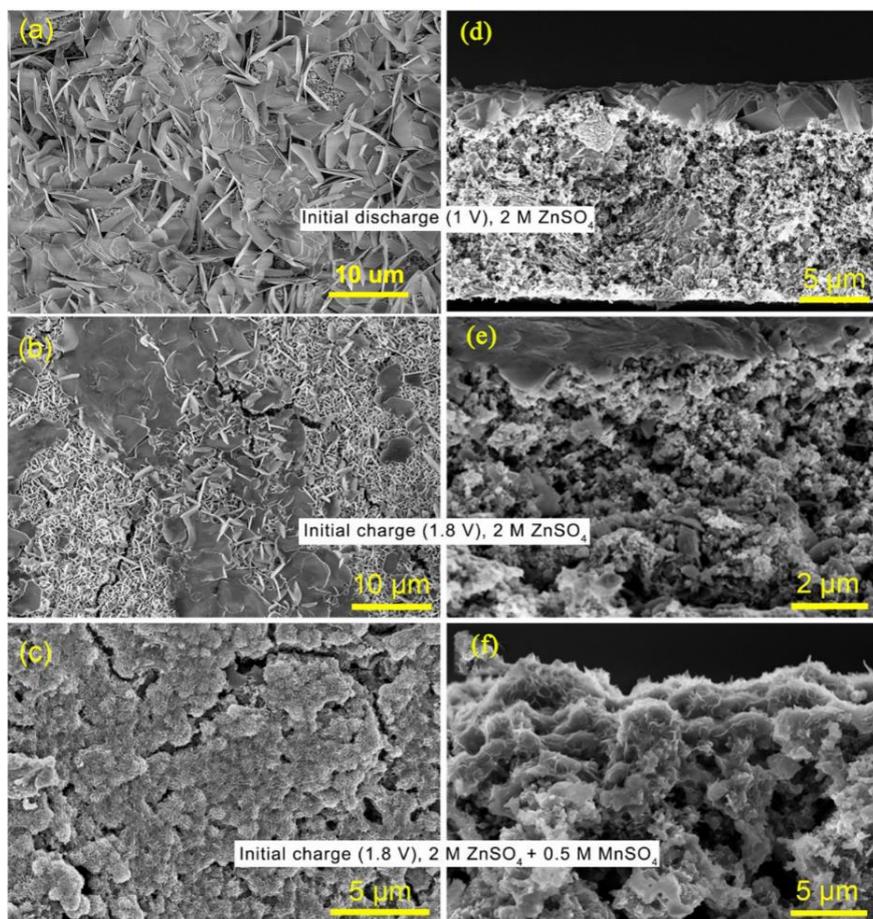
**Fig. S4** SEM- EDS and mapping result of the cathode which was constant current discharge to 1.4 V and constant voltage discharge at 1.4 V for 2 h



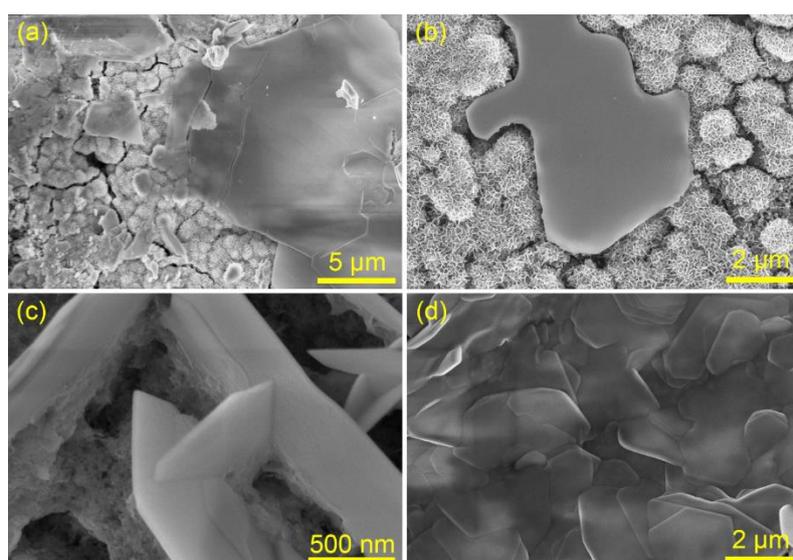
**Fig. S5** SEM-EDS result of the cathode which has been immersed in the electrolyte for 2 days before cleaned with deionized water



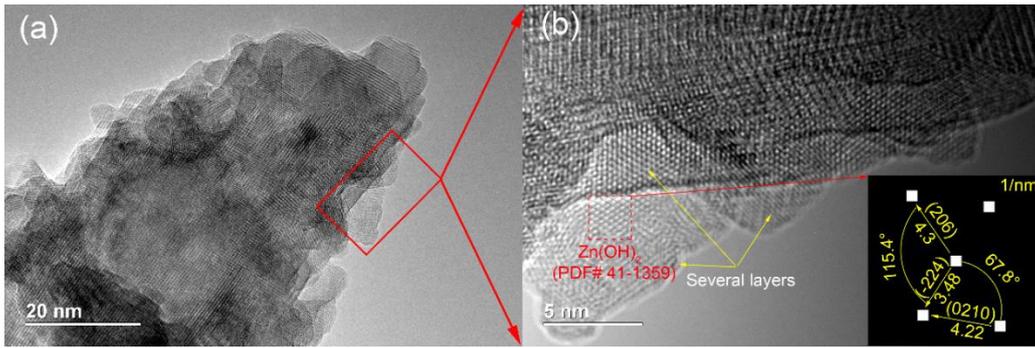
**Fig. S6** SEM-EDS mapping of the region in which the hexagonal plates have a radial distribution. **a** SEM image. **b, c, e, f** The distribution of O, Mn, S, and Zn. **d** EDS spectrum



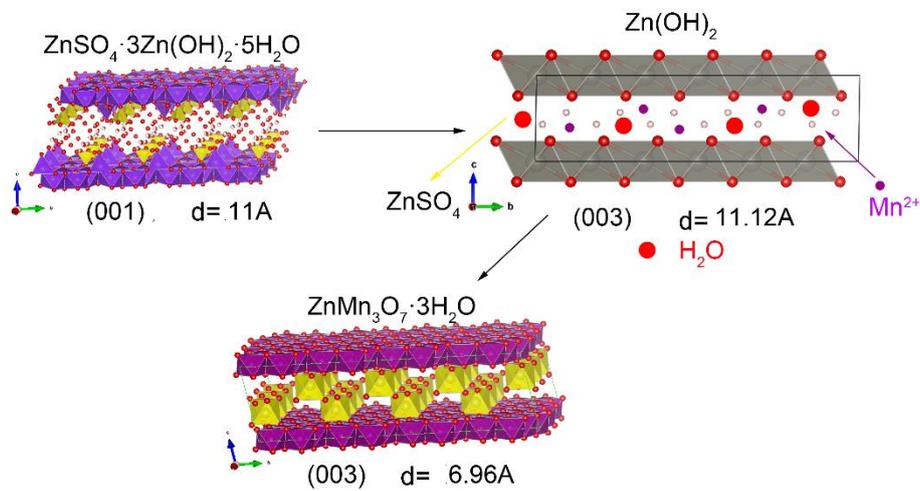
**Fig. S7** SEM results of  $\alpha$ - $\text{MnO}_2$  electrodes in different states, **a-c** the images of plane SEM images and **d-f** the section SEM image: **a, d** initial discharge; **b, e** initial charge in solution not added  $\text{Mn}^{2+}$ ; **c, f** initial charge in solution added  $\text{Mn}^{2+}$



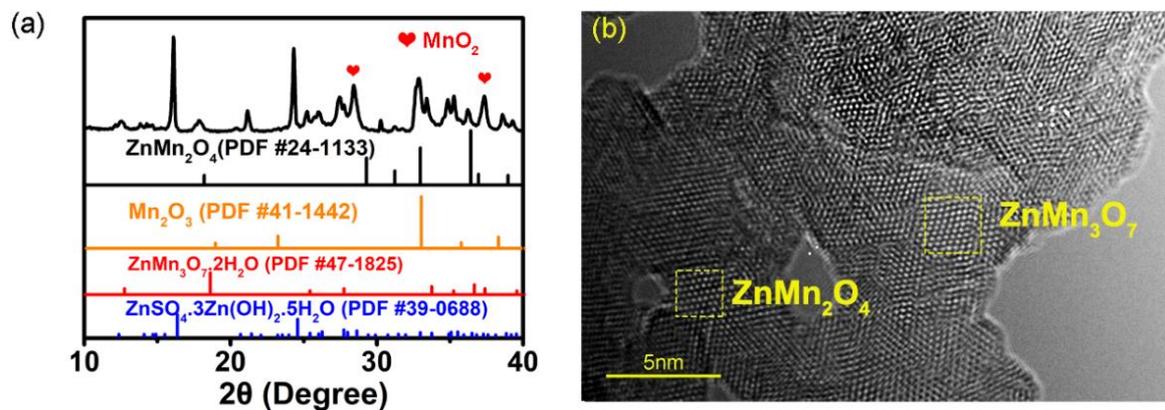
**Fig. S8** SEM of dissolution of BZSP in the initial charge process



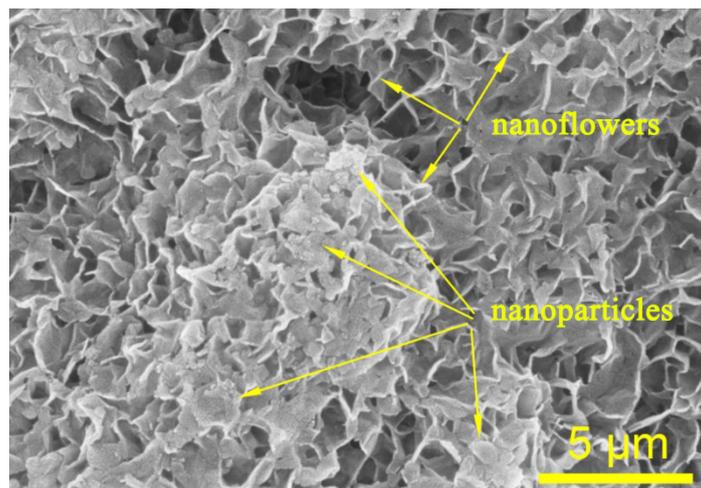
**Fig. S9** **a** TEM **b** high-resolution TEM (HRTEM) images. Element content in electrodes and electrolytes was analyzed by inductively coupled results of nanorods after 1.5 V constant voltage charge



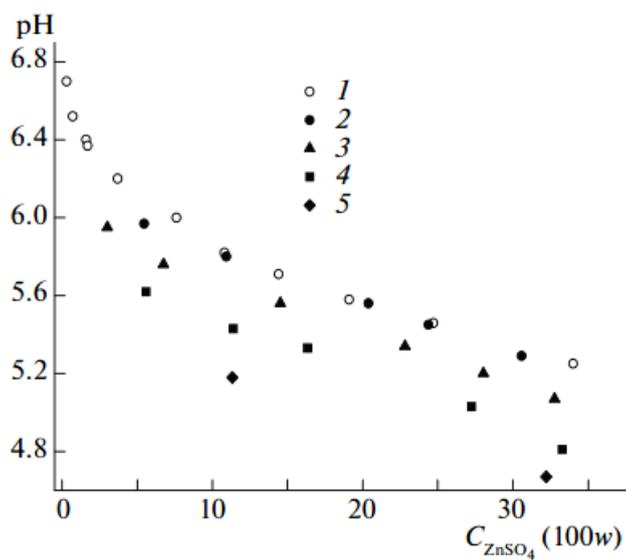
**Fig. S10** Schematic diagram of transitions between BZSP and  $\text{ZnMn}_3\text{O}_7 \cdot 3\text{H}_2\text{O}$



**Fig. S11** The cathode after 100 charges/discharge cycles in 2 M  $\text{ZnSO}_4$  electrolyte: **a** XRD pattern and **b** TEM image



**Fig. S12** SEM images of the structure generated during the process of the cycle



**Fig. S13** The relationship between the concentration of ZnSO<sub>4</sub> and pH of the solution in the ZnSO<sub>4</sub>-Zn(OH)<sub>2</sub>-H<sub>2</sub>O system at (1, 2) 291.15, (3) 298.15, (4) 308.15, and (5) 323.15 K. The figure is copied from Wu's work [S2]

**Table S1** Plasma atomic emission spectrometry (ICP-AES) results

Sample	Element content		
	Mn (ppm)	K (ppm)	Zn (ppm)
1. the original cathode	37.2	4.6	--
2. the cathode constant-current discharged from OCV to 1.0 V	23.4	2.3	63.2
3. the cathode constant-voltage discharged at 1.4 V for 4 hours	36.7	2.4	2.9
4. the electrolyte with sample 2	12.4	2.1	12950

**Table S2** Calculation procedures of fast Fourier transform (FFT) in Fig. 4e

$\alpha$ -MnOOH (PDF #24-0713)			Experiment			
Face	d (Å)	Angel (degree)	Length (nm)	Face	Angel (degree)	
FFT of 4e	{120}	3.4715	<(021),(101)>=41.77	a=1/0.3612	(1-20)	∠A=39.62
	{101}	2.4288	<(021),(1-20)>=107.86	c=1/0.2369	(101)	∠C=76.36
	{021}	2.5294	<(101),(1-20)>=66.08	b=1/0.2487	(021)	∠B=64.02

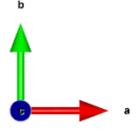
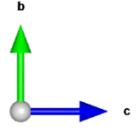
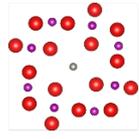
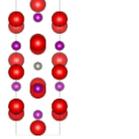
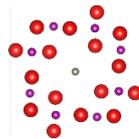
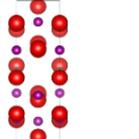
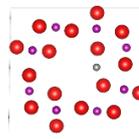
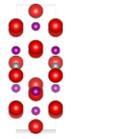
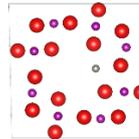
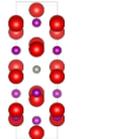
**Table S3** Calculation procedures of FFT in Fig. 4f-g

Mn <sub>2</sub> O <sub>3</sub> (PDF #41-1442)			Experiment			
Face	d (Å)	Angel (degree)	Length (nm)	Face	Angel (degree)	
FFT of 4f	{222}	2.7160	<(2-2-2),(400)>=54.73	a=1/0.2729	(222)	∠A=55.46
	{400}	2.3540	<(2-2-2),(222)>=109.47	c=1/0.2412	(400)	∠C=77.01
	{222}	2.7160	<(400),(222)>=54.74	b=1/0.2713	(2-2-2)	∠B=55.42
FFT of 4g	{222}	2.7160	<(321),(14-1)>=50.95	a=1/0.2719	(2-22)	∠A=52.07
	{321}	2.5140	<(2-22),(14-1)>=122.98	c=1/0.2546	(321)	∠C=57.23
	{411}	2.2194	<(2-22),(321)>=72.02	b=1/0.2306	(14-1)	∠B=70.70

**Table S4** Calculation procedures of FFT in Fig. 4h

$\alpha$ -MnO <sub>2</sub> (PDF #44-0141)			Experiment			
Face	d (Å)	Angel (degree)	Length (nm)	Face	Angel (degree)	
FFT of 4h	{310}	3.0930	<(211),(3-21)>=39.39	a=1/0.3083	(-130)	∠A=39.62
	{321}	1.9699	<(-130),(3-21)>=124.95	c=1/0.2440	(211)	∠C=57.02
	{211}	2.3950	<(-130),(211)>=85.56	b=1/0.2024	(3-21)	∠B=83.36

**Table S5** Calculation results of inserting one  $Zn^{2+}$  into one  $\alpha$ - $MnO_2$  cell

Site	Wyckoff Position			a (Å)	b (Å)	c (Å)	$\Delta V$ (%)	$\Delta E$ (eV)
2a	(0.5,0.5,0.5)			9.71	9.71	3.01	-1.13	-1.23
2b	(0.5,0.5,0)			9.93	9.93	2.93	0.78	-0.2
8h	(0.6,0.5,0)			10.41	9.56	2.95	2.44	-1.58
8h'	(0.6,0.5,0.5)			10.02	10.08	2.96	4.01	-1.34

**Table S6** Six possible electrochemical reduction routes of  $MnO_2$  as cathode Zn-Mn- $H_2O$  system

Mechanism	Reaction in cathode	Reaction type	Cathode Potential	
			(V vs. SHE)	E (V)
Proton-electron conversion	$MnO_2 + H^+ + e^- = MnOOH$	Heterogeneous reaction	$\psi^+ = 1.036 - 0.0592pH$	1.47
Proton-electron	$MnO_2 + xH^+ + xe^- = H_xMnO_2$	Homogeneous reaction	$\psi^+ = E - \psi$	$E = -\Delta E_f / e$
Manganese oxide conversion	$2MnO_2 + 2H^+ + 2e^- = Mn_2O_3 + H_2O$	Heterogeneous reaction	$\psi^+ = 0.974 - 0.0592pH$	1.41
$Mn^{2+}$	$MnO_2 + 4H^+ + 2e^- = Mn^{2+} + 2H_2O$	Heterogeneous reaction	$\psi^+ = 1.23 + 0.03 \log a_{Mn^{2+}} - 0.12pH$	Determined by $a_{Mn^{2+}}$ and pH
Zinc ion insertion conversion	$Zn^{2+} + 2MnO_2 + 2e^- = ZnMn_2O_4$	Heterogeneous reaction	$\psi^+ = 0.76 - 0.03 \lg a_{Zn^{2+}}$	1.52

Zinc ion insertion	$x\text{Zn}^{2+} + \text{MnO}_2 + 2xe^- = \text{Zn}_x\text{MnO}_2$	Homogeneous reaction	$\psi^+ = E - \psi^-$	$E = \Delta E_f / e1.58$ ( $x = 0.125$ )
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**Table S7**  $\Delta G$  data of some possible species in Zn-Mn-H<sub>2</sub>O system

Species	$\Delta G$ (kcal mol <sup>-1</sup> )*
H <sub>2</sub> O	-56.678
Mn <sup>2+</sup>	-54.493
MnO	-86.719
Mn(OH) <sub>2</sub>	-147.176
Mn <sub>3</sub> O <sub>4</sub>	-306.654
MnOOH	-135.547
Mn <sub>2</sub> O <sub>3</sub>	-210.557
ZnMn <sub>2</sub> O <sub>4</sub>	-293.439
MnO <sub>2</sub>	-111.65
Zn <sup>2+</sup>	-35.194
ZnO	-76.571
Zn(OH) <sub>2</sub>	-132.309
MnO <sub>4</sub> <sup>-</sup>	-106.836
Zn	0
Mn	0

\*  $T = 298.15$  K;  $p = 1$  bar; data from the HSC Chemistry software.

## Supplementary References

- [S1] H. Pan, Y. Shao, P. Yan, Y. Cheng, K.S. Han et al., Reversible aqueous zinc/manganese oxide energy storage from conversion reactions. *Nat. Energy* **1**, 16039 (2016). <https://doi.org/10.1038/nenergy.2016.39>
- [S2] X. Wu, X. Yin, Z. Chen, X. Yu, D. Zeng, Y. Tan, Experimental determination and model simulation of the solid-liquid equilibria in the ZnSO<sub>4</sub>-Zn(OH)<sub>2</sub>-H<sub>2</sub>O system. *Russ. J. Phys. Chem. A* **89**, 958-962 (2015). <https://doi.org/10.1134/S0036024415060345>